



Polymer injection molding simulations in OpenFOAM®

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- Injection molding
 - Communication
 - Medicine
 - Automotive
 - Packaging
 - etc...
- Expensive development stage
 - high pressure
 - high clamping forces
 - high viscosity
- Simulation
 - PolyFlow, Sigmasoft, Moldex3D, ...
 - OpenFOAM®
- Model implementation
 - compressibility (pVT)
 - viscosity (non-Newtonian)



Incompressible models:*powerLaw:*

$$\nu(\dot{\gamma}) = \nu_0 \dot{\gamma}^{n-1}$$

CrossPowerLaw:

$$\nu(\dot{\gamma}) = \frac{\nu_0 - \nu_\infty}{1 + (m\dot{\gamma})^n} + \nu_\infty$$

BirdCarreau:

$$\nu(\dot{\gamma}) = \nu_\infty + (\nu_0 - \nu_\infty) \left(1 + (m\dot{\gamma})^a\right)^{\frac{n-1}{a}}$$

$$\nu = \nu(\dot{\gamma}, T, p)$$

Compressible models:*perfectFluid:*

$$\rho(p) = \rho_0 + \frac{p}{RT}$$

adiabaticPerfectFluid:

$$\rho(p) = \rho_0 \left(\frac{p+B}{p_0+B}\right)^{\frac{1}{\gamma}}$$

$$\rho = \rho(T, p)$$

VOF:

$$\rho = \alpha\rho_l + (1 - \alpha)\rho_g$$
$$\frac{\partial\alpha}{\partial t} + \nabla \cdot (\alpha\mathbf{u}) + \nabla \cdot (\alpha(1 - \alpha)\mathbf{u}_r) = S_p + S_u$$

Continuity equation:

$$\frac{\partial\rho\mathbf{u}}{\partial t} + \nabla \cdot (\rho\mathbf{u}) = 0$$

Momentum equations:

$$\frac{\partial\rho\mathbf{u}}{\partial t} + \nabla \cdot (\rho\mathbf{u}\mathbf{u}) = -\nabla p + \nabla \cdot \boldsymbol{\tau} + \rho\mathbf{g} + \mathbf{F}_\sigma$$

Energy equation:

$$\frac{\partial\rho T}{\partial t} + \nabla \cdot (\rho\mathbf{u}T) =$$
$$\Delta(\bar{k}T) + \boldsymbol{\tau} : \nabla\mathbf{u} \cdot \left(\frac{\alpha}{c_{v_1}}\right) + [\nabla \cdot (\rho\mathbf{u})] \left(\frac{\alpha}{c_{v_1}} + \frac{(1-\alpha)}{c_{v_2}}\right)$$

tempPowerLaw (first order):

$$\nu(\dot{\gamma}, T) = \nu_0 \dot{\gamma}^{n-1} e^{c \cdot (T - T_0)}$$

$$\nu = \nu(\dot{\gamma}, T, p)$$

CarreauYasudaWLF:

$$\nu(\dot{\gamma}, T) = \nu_\infty \cdot a_T(T) + (\nu_0 - \nu_\infty) a_T(T) (1 + (\lambda a_T(T) \dot{\gamma})^a)^{\frac{n-1}{a}}$$

$$\log a_T(T) = \frac{8.86 \cdot (T_0 - T_S)}{101.6 + (T_0 - T_S)} - \frac{8.86 \cdot (T - T_S)}{101.6 + (T - T_S)}$$

CrossArrhenius:

$$v(\dot{\gamma}, T) = \frac{v_0(T)}{1 + \left(\frac{v_0(T)\dot{\gamma}}{\tau^*}\right)^{1-n}}$$

$$v = v(\dot{\gamma}, T, p)$$

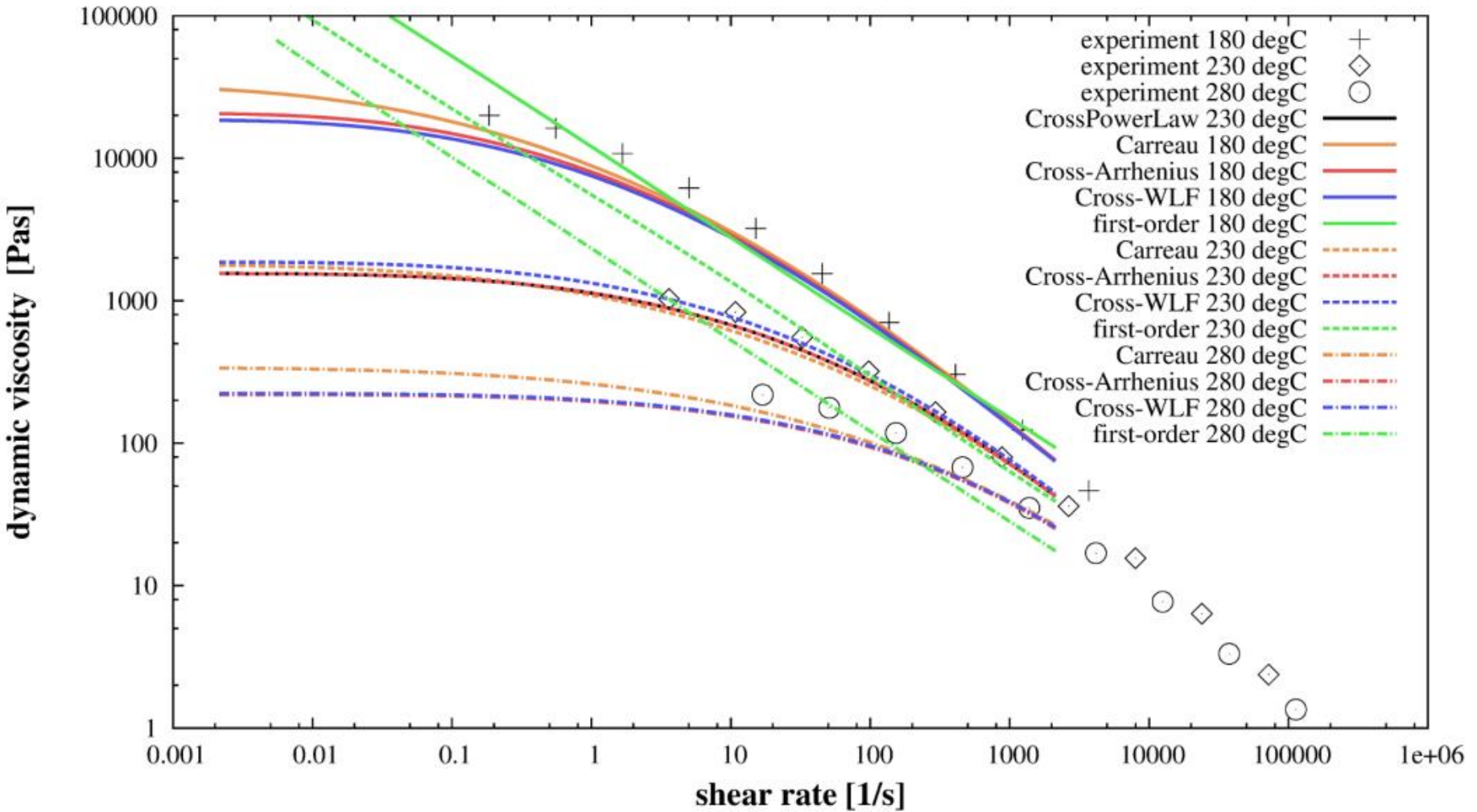
$$v_0(T) = B \cdot e^{T_b/T}$$

CrossWLF:

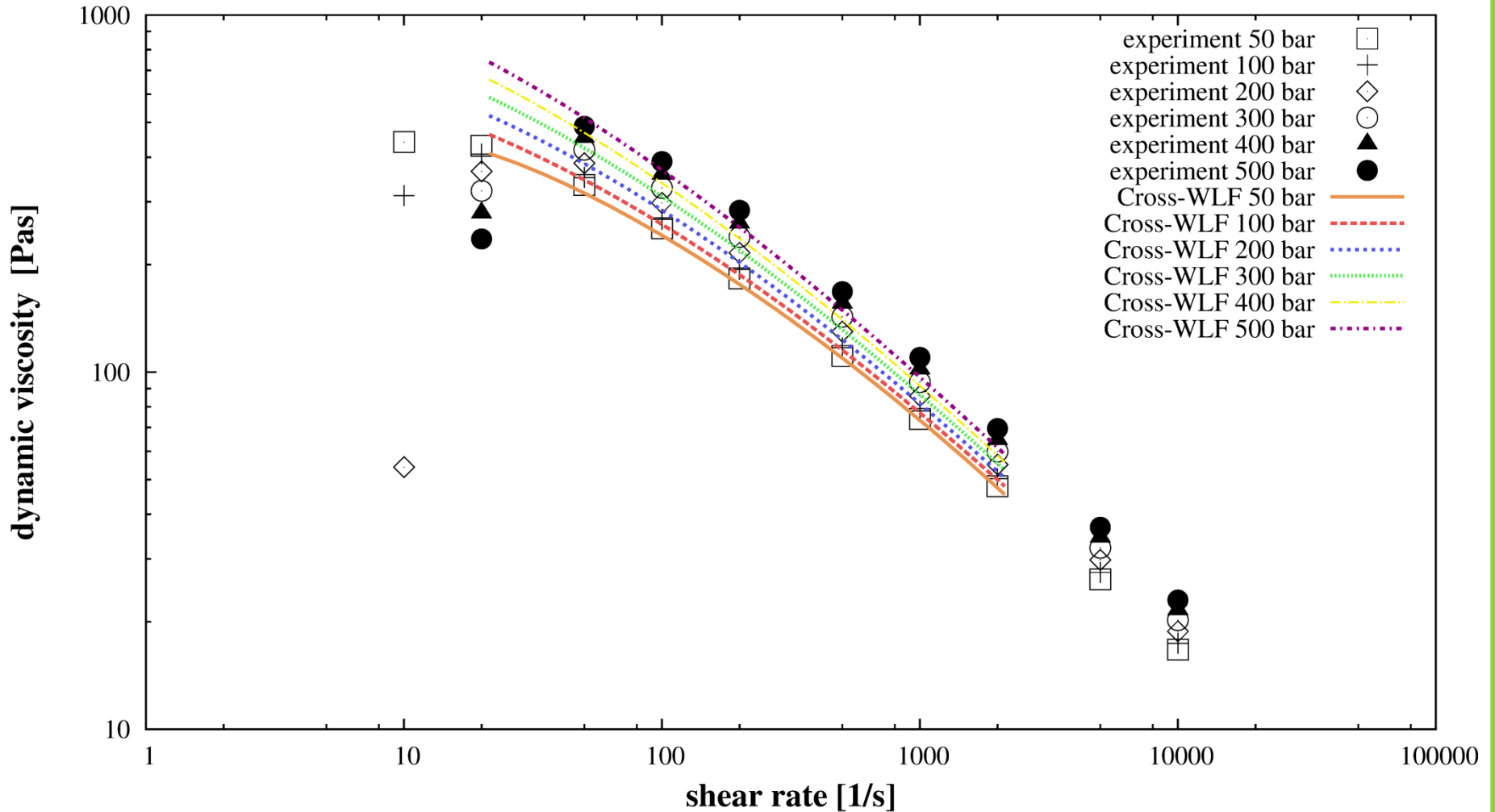
$$v(\dot{\gamma}, T, p) = \frac{v_0(T, p)}{1 + \left(\frac{v_0(T, p)\dot{\gamma}}{D_4}\right)^{1-n}}$$

$$v_0(T) = D_1 \cdot \exp\left(\frac{(-A_1) \cdot (T - D_2 - D_3 \cdot p)}{A_2 + T - D_2 - D_3 \cdot p}\right)$$

PS – 145D



PP – HG313MO



Schmidt:

$$v(p, T) = \frac{PF1}{PF4+p} + \frac{PF2 \cdot T}{PF3+p} \quad T \leq T_{trans}$$

$$v(p, T) = \frac{PS1}{PS4+p} + \frac{PS2 \cdot T}{PS3+p} \quad T \geq T_{trans}$$

$$T_{trans} = PK1 + PK2 \cdot p$$

$$\rho = \rho(T, p)$$

Tait:

$$v(p, T) = \left\{ v_s(T) \cdot \left[1 - C \cdot \ln \left(1 + \frac{p}{B_s(T)} \right) \right] + W_s(T) \right\} \quad T \leq T_{trans}$$

$$v_s(T) = b_{1s} + b_{2s} \cdot (T - b_5)$$

$$B_s(T) = b_{3s} \cdot e^{-b_{4s} \cdot (T - b_5)}$$

$$W_s(T) = b_7 \cdot e^{b_8 \cdot (T - b_5) - b_9 \cdot p}$$

$$v(p, T) = \left\{ v_m(T) \cdot \left[1 - C \cdot \ln \left(1 + \frac{p}{B_m(T)} \right) \right] \right\} \quad T \geq T_{trans}$$

$$v_m(T) = b_{1m} + b_{2m} \cdot (T - b_5)$$

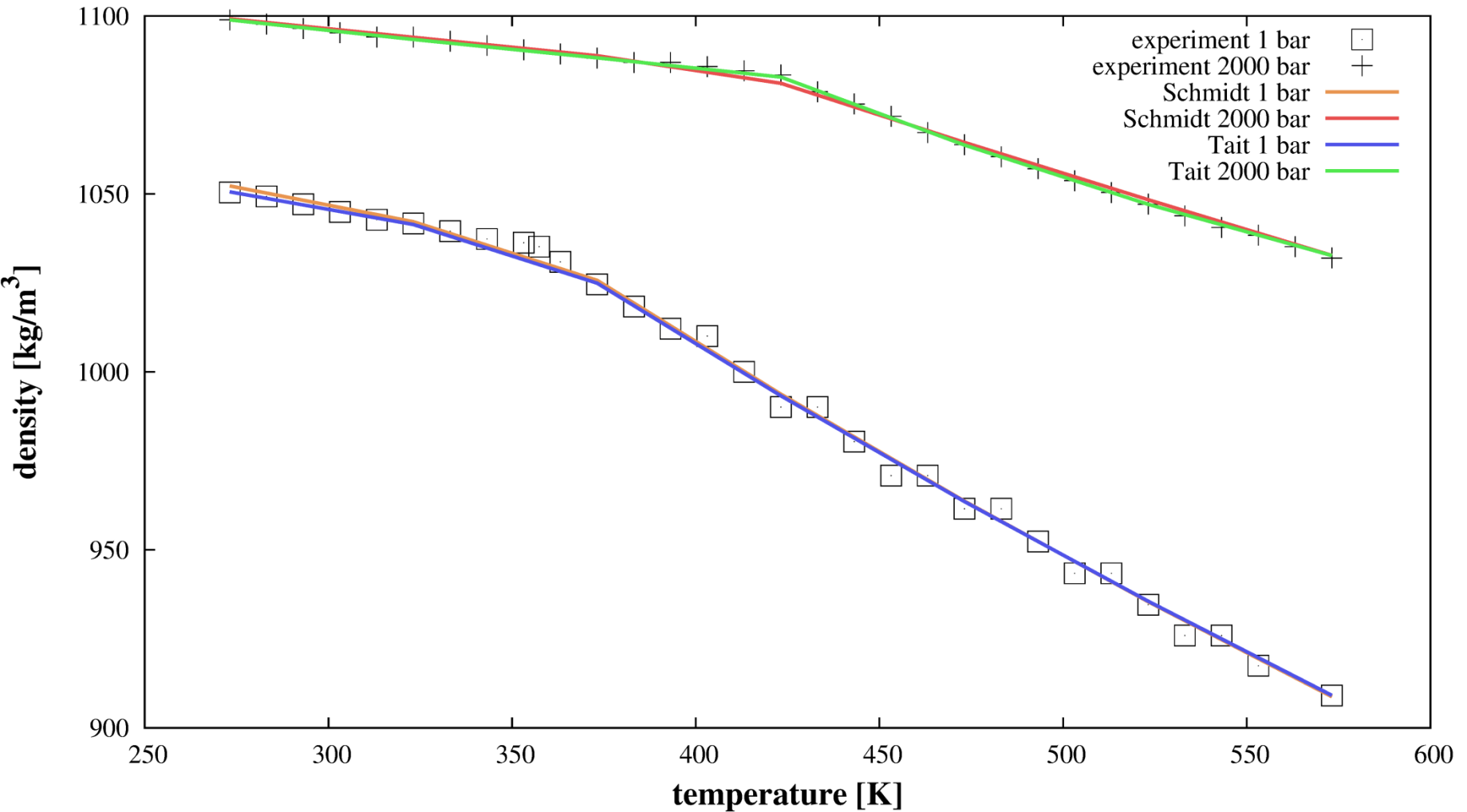
$$B_m(T) = b_{3m} \cdot e^{-b_{4m} \cdot (T - b_5)}$$

$$T_{trans} = b_5 + b_6 \cdot p$$

$$\rho = \rho(T, p)$$

$$C = 0.0894$$

PS – 145D



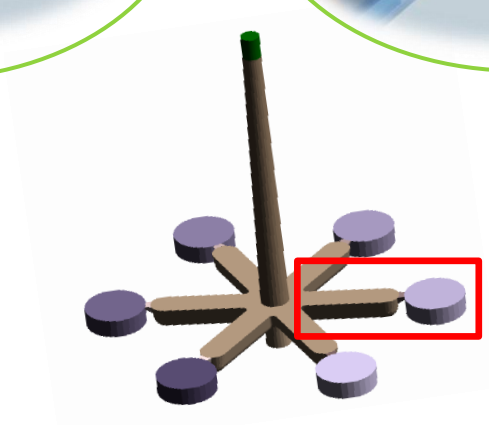
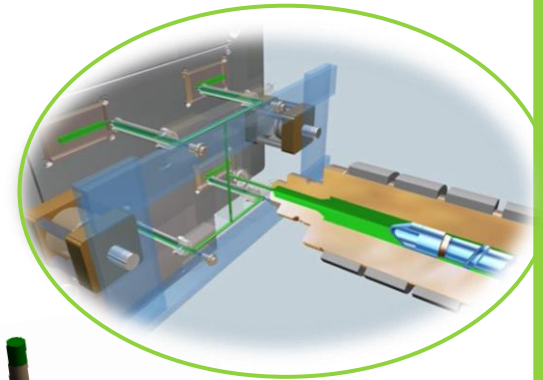
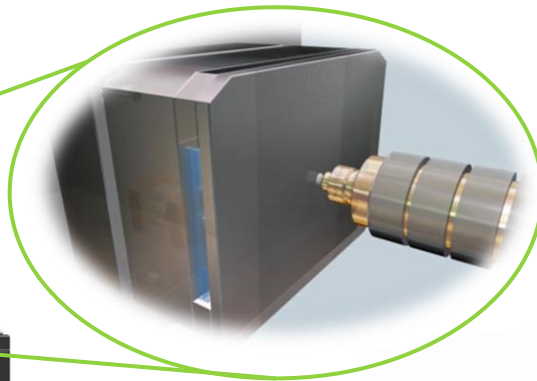
Discontinuous processing technique for polymer-additive systems

Injection molding machine:

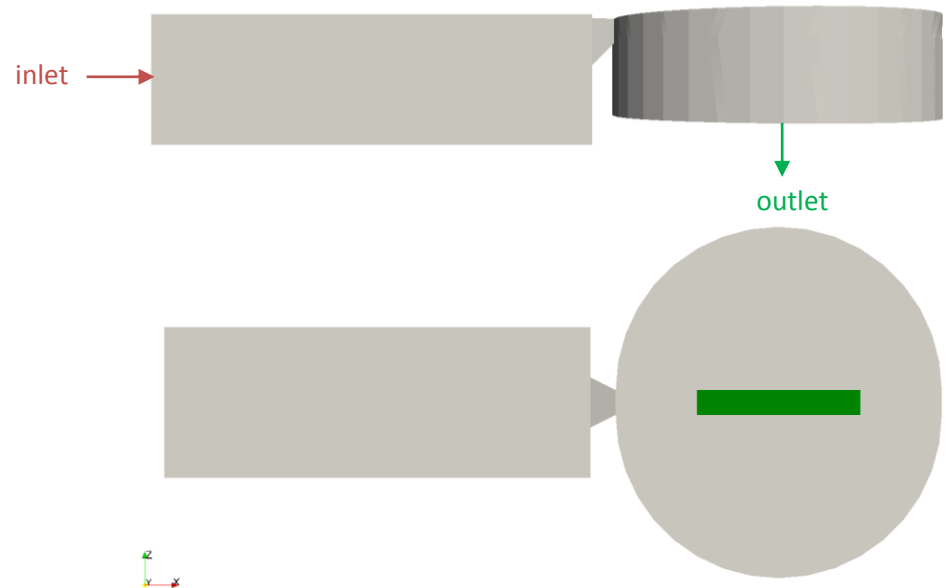
- Plasticizing the polymer-additive system with single screw
- Shaping of the melt within the cavities in the mold
- One-stop production

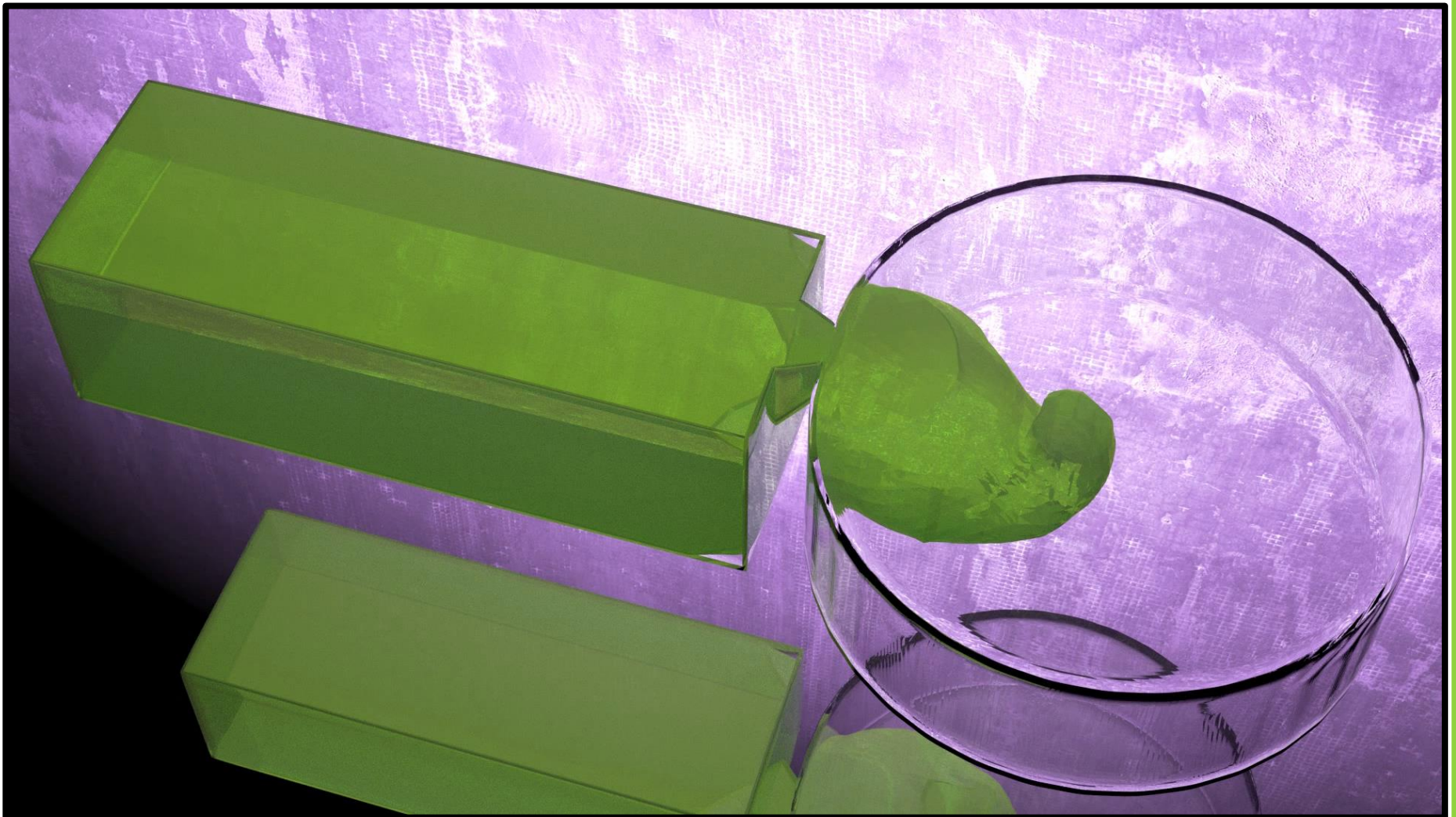


Injection Molding Machine type e-mac; Source: ENGEL Austria GmbH



- Trial simulation of injection process (coarse mesh)
 - Influence of strain rate, density, temperature, pressure, viscosity etc.
 - Back coupling
- Geometry – 1 tablet cavity
- Fill time of **1s**
- Wall temperature of **503 K**
- Inlet temperature of **553 K**
- Tait, CrossWLF for PS 145D





t = 0.25s



t = 0.75s



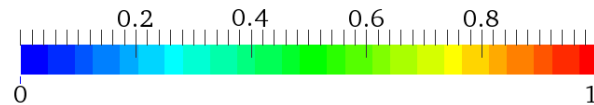
t = 0.5s



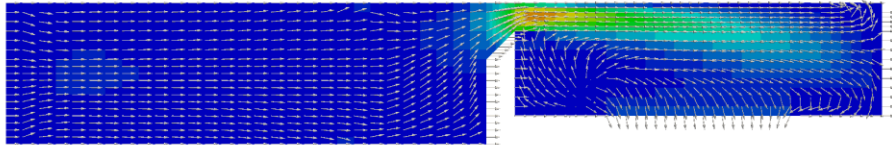
t = 1s



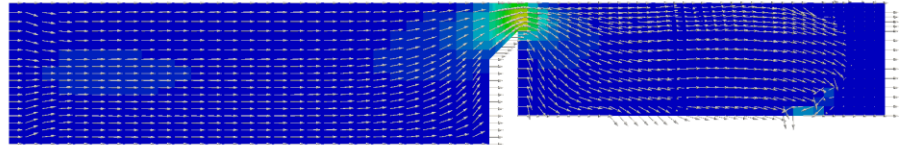
liquid phase fraction [-]



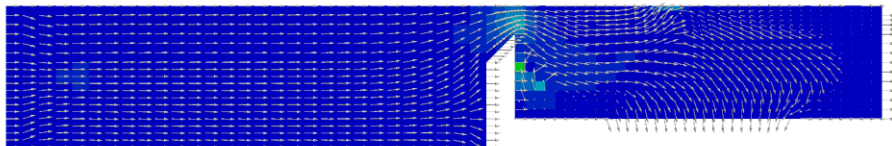
t = 0.25 s



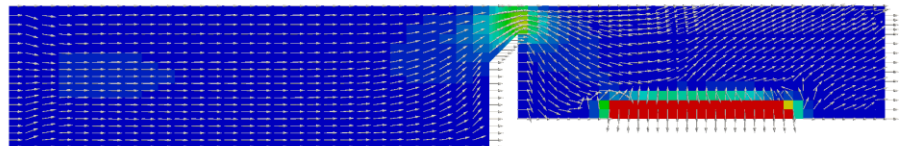
t = 0.75 s



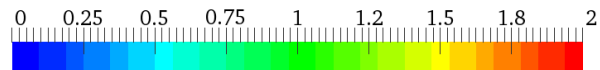
t = 0.5 s



t = 1 s



velocity magnitude [m/s]



$t = 0.25\text{ s}$



$t = 0.75\text{ s}$



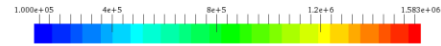
pressure [Pa]



$t = 0.5\text{ s}$



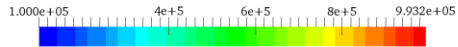
pressure [Pa]



$t = 1\text{ s}$



pressure [Pa]



pressure [Pa]



t = 0.25 s



t = 0.75 s



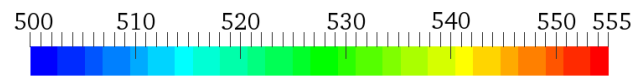
t = 0.5 s



t = 1 s



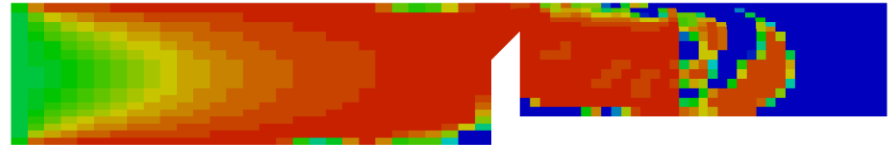
temperature [K]



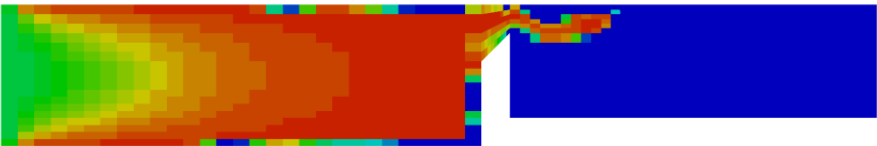
t = 0.25 s



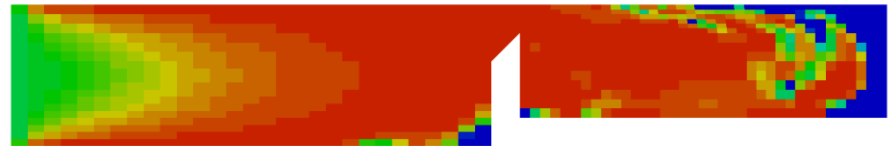
t = 0.75 s



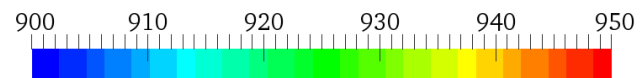
t = 0.5 s



t = 1 s



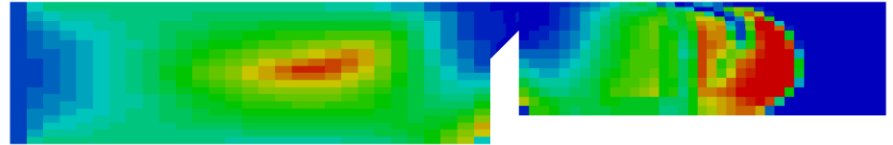
density [kg/m³]



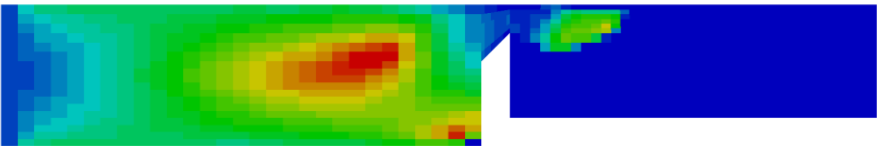
t = 0.25 s



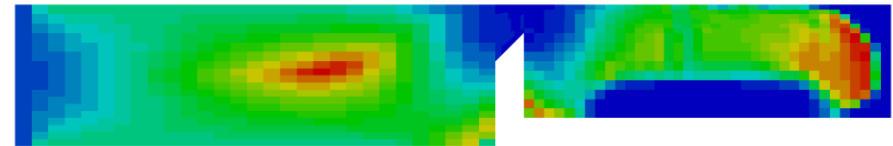
t = 0.75 s



t = 0.5 s



t = 1 s



dynamic viscosity [Pas]



- Injection molding process in OpenFOAM®
- Implemented viscosity models
 - tempPowerLaw (first order)
 - CarreauYasudaWLF
 - CrossArrhenius
 - CrossWLF
- Implemented compressibility models
 - Schmidt
 - Tait
- Adaptation of compressibleInterFoam
- Next steps
 - crystallization
 - fiber orientation
 - cure
 - etc...

Thank you for your attention!

Introduction to injection molding technique and its simulation

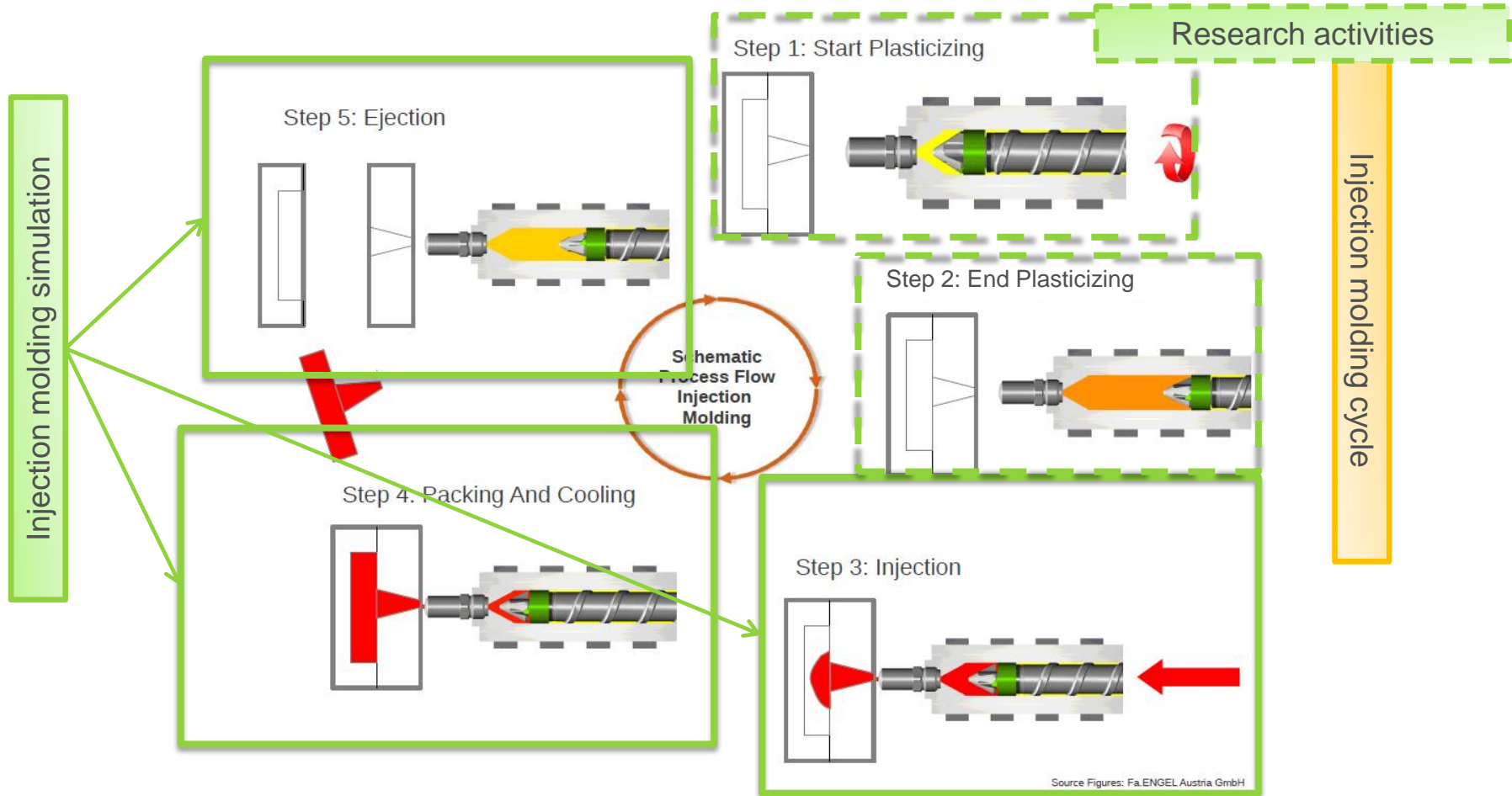


Figure 2: Injection molding cycle